# The effect of surface-charge convection on the settling velocity of spherical drops in a uniform electric field

# EHUD YARIV<sup>1</sup> AND YANIV ALMOG<sup>2</sup>

<sup>1</sup>Department of Mathematics, Technion — Israel Institute of Technology, Haifa 32000, Israel <sup>2</sup>Department of Mathematics, Louisiana State University, Baton Rouge, Louisiana 70803, USA

#### (Received 11 April 2016)

The mechanism of surface-charge convection, quantified by the electric Reynolds number Re, renders the Melcher–Taylor electrohydrodynamic model inherently nonlinear, with the electrostatic problem coupled to the flow. Because of this nonlinear coupling, the settling speed of a drop under a uniform electric field differs from that in its absence. This difference was calculated by Xu & Homsy (J. Fluid Mech., vol. 564, 2006, pp. 395–414) assuming small Re. We here address the same problem using a different route, considering the case where the applied electric field is weak, in the sense that the magnitude of the associated electrohydrodynamic velocity is small compared with the settling velocity. As convection is determined at leading order by the well-known flow associated with pure settling, the electrostatic problem becomes linear for arbitrary value of Re. The electrohydrodynamic correction to the settling speed is then provided as a linear functional of the electric-stress distribution associated with that problem. Calculation of the settling speed eventually amounts to the solution of a difference equation governing the respective coefficients in a spherical-harmonics expansion of the electric potential. It is shown that, despite the present weak-field assumption, our model reproduces the small-Re approximation of Xu & Homsy as a particular case. For finite Re, inspection of the difference equation reveals a singularity at the critical value

$$Re = \frac{4S(1+R)(1+M)}{(1+S)M},$$

wherein R, S and M respectively denote the ratios of resistivity, permittivity and viscosity values in the suspending- and drop phases, as defined by Melcher & Taylor (*Ann. Rev. Fluid Mech.*, vol. 1, 1969, pp. 111–146). Straightforward numerical solutions of this equation for electric Reynolds numbers smaller than the critical value reveal a non-monotonic dependence of the settling speed upon the electric-field magnitude, including a transition from velocity enhancement to velocity decrement.

#### 1. Introduction

While surface-charge convection (SCC) explicitly appears in the leaky-dielectric model of Melcher & Taylor (1969), this mechanism is neglected in the three steady-state illustrations provided in that review, the third being Taylor's classical analysis of the electrohydrodynamic flow about a drop in a uniform electric field (Taylor 1966). It appears that this neglect has been motivated, at least partially, by its mere convenience. Indeed, in the absence of of SCC the electrostatic problem becomes linear, allowing for simple analytic solutions.

The nonlinear SCC mechanism is quantified by the electric Reynolds number Re,

#### E. Yariv and Y. Almog

representing the ratio of charge convection to Ohmic conduction. The classical analysis of Taylor (1966) thus applies for Re = 0. It appears that the first attempt to analyse the role of SCC in Taylor's problem was by Feng (1999), using both a perturbative analysis for  $Re \ll 1$  and a numerical finite-element scheme for finite Re. More recently, the finite-Re problem was revisited by Lanauze, Walker & Khair (2015) using a boundary-integral method, allowing to reach larger values of Re. Both papers have also considered the effect of deformations from a spherical shape, another feature absent in Taylor's analysis.

Due to their inherent fore–aft symmetry, electrohydrodynamic flows about spherical drops cannot be naturally described using any single scalar property. (When deformation is allowed, one may employ the deviation from sphericity as the requisite scalar measure.) This has motivated the analysis of Xu & Homsy (2006) who considered a drop under both gravity and applied field. In the absence of SCC, the electrostatic problem is decoupled from the hydrodynamic one, which accordingly represents a simple superposition of the familiar flow associated with a settling drop (under an imposed external force) and the 'pure' electrohydrodynamic flow of Taylor (1966). Due to the fore–aft symmetry of the latter, the settling velocity of the drop is unaffected by the applied field. In the presence of SCC, however, the electrostatic and hydrodynamic problems are mutually (and nonlinearly) coupled. The settling velocity then depends upon the applied-field magnitude, and may therefore constitute a scalar measure of the intensity of the electrohydrodynamic flow.

Xu & Homsy (2006) implicitly considered the general case where the settling velocity is comparable with the electrohydrodynamic scale. To facilitate analytic progress, they assumed that the electric Reynolds number is small. This allows for a regular-perturbation analysis, where the perturbation due to SCC gives rise to velocity correction proportional to Re. We propose here a different route. Consider the case where the applied field is weak, in the sense that the electrohydrodynamic velocity scale is small compared with the settling speed. Surface convection is then dominated by the velocity field associated with a settling drop, in the absence of electrohydrodynamic effects. The electrostatic problem is then *linear* at leading order for arbitrary values of Re. Once it is solved, the resulting electric shear stresses may be readily utilised to calculate the electrohydrodynamic correction to the settling velocity. To focus upon the SCC mechanism we assume that surface tension is strong enough to retain an approximately spherical shape.

The paper is arranged as follows. In the next section we formulate the exact nonlinear problem governing the electric and flow fields. In §3 we then derive several general properties of this problem, valid for arbitrary values of the applied fields. Our solution scheme for weak applied field is outlined in §4, and the associated linear electrostatic problem is analysed in §5. The limit of small Re is discussed in §6, showing — perhaps counter-intuitively — that the drop velocity calculated by Xu & Homsy (2006) is reproduced within the present scheme. The calculation of the drop velocity for arbitrary values of Re is discussed in §7, where we show that solutions exists only below a critical value of Re. The respective assumptions and approximation underlying our analysis are scrutinised in §8. We conclude in §9, pointing out a range of open problems.

# 2. Problem formulation

A leaky-dielectric Drop (permittivity  $\bar{\epsilon}^*$ , conductivity  $\bar{\sigma}^*$ , viscosity  $\bar{\mu}^*$ ) is suspended in another leaky-dielectric liquid (permittivity  $\epsilon^*$ , conductivity  $\sigma^*$ , viscosity  $\mu^*$ ) of an unbounded extent. (Hereafter an asterisk is used to decorate dimensional quantities; the bar decoration is employed for drop-phase variables.) The drop settles due to gravity in a direction specified by the unit-vector  $\hat{\imath}$ . (When the drop density  $\bar{\rho}^*$  is larger than the density  $\rho^*$  of the suspending liquid, this is the gravity direction; if  $\bar{\rho}^* < \rho^* \hat{\imath}$  is in the opposite direction.) In addition, it is exposed to a uniformly applied electric field of magnitude  $E^*$  in that direction. We assume that capillarity is sufficiently strong to maintain an approximately spherical drop, say of radius  $a^*$ . Our interest is in the steadystate solution, and in particular in the settling speed.

The problem is characterised by two velocity scales. The first is the settling velocity in the absence of an applied field, namely

$$\mathcal{U}^* = \frac{1}{3} \frac{M+1}{M+3/2} \frac{|\bar{\rho}^* - \rho^*| g^* a^{*2}}{\mu^*}, \qquad (2.1)$$

where  $M = \mu^* / \bar{\mu}^*$  and  $g^*$  is the acceleration due to gravity. The second is the electrohydrodynamic velocity

$$\frac{\epsilon^* a^* E^{*2}}{\mu^*}.\tag{2.2}$$

We employ a dimensionless notation, where length variables are normalised by  $a^*$ , velocity variables by  $\mathcal{U}^*$  and electric fields by  $E^*$ . The electric potentials (normalised by  $a^*E^*$ ) in the medium and drop phases are respectively denoted by  $\varphi$  and  $\bar{\varphi}$ ; the corresponding velocity fields are denoted by  $\boldsymbol{u}$  and  $\bar{\boldsymbol{u}}$ . The dimensionless problem governing these fields depends upon: (i) the ratio of the two velocity scales,

$$W = \frac{\epsilon^* a^* E^{*2}}{\mu^* \mathcal{U}^*}; \tag{2.3}$$

(ii) the material ratios  $R = \bar{\sigma}^*/\sigma^*$ ,  $S = \epsilon^*/\bar{\epsilon}^*$  and  $M = \mu^*/\bar{\mu}^*$ ; and (iii) the electric Reynolds number, provided by the ratio of the charge relaxation time  $\epsilon^*/\sigma^*$  to the convective time  $a^*/\mathcal{U}^*$ :

$$Re = \frac{\epsilon^* \mathcal{U}^*}{a^* \sigma^*}.$$
(2.4)

The problem is formulated in a drop-fixed reference system, using spherical coordinates  $(r, \theta, \varpi)$  with the radial coordinate r measured from the drop centre and the latitudinal angle  $\theta$  measured from the direction specified by  $\hat{\imath}$ . The corresponding unit vectors are denoted  $(\hat{e}_r, \hat{e}_{\theta}, \hat{e}_{\varpi})$ . Because of axial symmetry, the azimuthal angle  $\varpi$  is degenerate. The velocity fields in the suspending and drops phases are accordingly written  $u = \hat{e}_r u + \hat{e}_{\theta} v$  and  $\bar{u} = \hat{e}_r \bar{u} + \hat{e}_{\theta} \bar{v}$ .

The electrostatic problem consists of: (i) Laplace's equation outside and inside the drop; (ii) electric-potential continuity

$$\varphi = \bar{\varphi} \quad \text{at} \quad r = 1;$$
 (2.5)

(iii) regularity inside the drop; and (iv) the far-field condition

$$\varphi \sim -r\cos\theta \quad \text{as} \quad r \to \infty,$$
 (2.6)

corresponding to a unit field in the  $\hat{\pmb{\imath}}\text{-direction}.$  In addition, it also consists of the charging condition

$$\frac{\partial \varphi}{\partial r} - R \frac{\partial \bar{\varphi}}{\partial r} = \frac{Re}{\sin \theta} \frac{\partial}{\partial \theta} (qv \sin \theta) \quad \text{at} \quad r = 1,$$
(2.7)

wherein

$$q = S^{-1} \frac{\partial \bar{\varphi}}{\partial r} - \frac{\partial \varphi}{\partial r}$$
(2.8)

is the surface-charge density (normalised by  $\epsilon^* E^*$ ).

The SCC term in the right-hand side of (2.7) introduces a coupling to the velocity

field. The flow is governed by the continuity and Stokes equations in the two phases. At the drop boundary r = 1 it satisfies the kinematic condition of vanishing radial velocities,

$$u = \bar{u} = 0, \tag{2.9}$$

the dynamic condition of tangential-velocity continuity,

$$v = \bar{v} \tag{2.10}$$

(already tacitly used in (2.7)) and the shear-stress condition, balancing hydrodynamic viscous stresses with electric shear stresses,

$$\hat{\boldsymbol{e}}_r \cdot (\boldsymbol{S} - \bar{\boldsymbol{S}}) \cdot \hat{\boldsymbol{e}}_{\theta} = W q \frac{\partial \varphi}{\partial \theta}, \qquad (2.11)$$

wherein S and  $\overline{S}$  respectively denote the hydrodynamic stresses at the two phases. At large distances the velocity approaches a uniform velocity,

$$\boldsymbol{u} \to -U \boldsymbol{\hat{\imath}} \quad \text{as} \quad r \to \infty.$$
 (2.12)

The settling velocity U is determined by the condition that the sum of external and hydrodynamic forces on the drop vanishes, resulting in a nonlinear 'mobility' problem. In general, then, the settling velocity is a function of both W and Re, as well as the ratios R, S and M.

# 3. General properties

Due to the SCC term in (2.7) the problem is inherently nonlinear. No closed-form analytic solution is accordingly expected. (Note that no analytic solution is known even in the absence of gravity.) Nonetheless, there are three general observations which can be made immediately (cf. Yariv & Frankel 2016).

The first is that the net surface charge must vanish,

$$\oint_{r=1} q \,\mathrm{d}A = 0 \tag{3.1}$$

(wherein the areal element dA is normalised by  $a^{*2}$ ). Indeed, by Gauss law a net interfacial charge must be accompanied by a net electric flux through any closed surface which encloses the drop. Because of the Ohmic nature of the leaky-dielectric liquid, such a flux would be equivalent to a net electric current emanating from the drop, in contradiction to the assumed steady state. Mathematically, Laplace's equation inside the drop implies that the integral of  $\partial \bar{\varphi} / \partial r$  over the unit sphere r = 1 must vanish. The charging condition (2.7) then necessitates the same for  $\partial \varphi / \partial r$ . Using (2.8), (3.1) readily follows. The absence of charge in conjunction with Laplace's equation and the approach (2.6) to a uniform field implies that the drop does not experience any electric force (Rivette & Baygents 1996; Yariv 2006). It follows that the external force on the drop is only due to gravity.

The second observation is that in the absence of such an external force, the problem retains the familiar symmetry about the mid-plane  $\theta = \pi/2$ , implicit in the original problem of Taylor (1966). Thus, under the reflection  $\theta \to \pi - \theta$  the pertinent fields transform as

$$(\varphi,\bar{\varphi}) \to (-\varphi,-\bar{\varphi}), \quad q \to -q, \quad (u,\bar{u}) \to (u,\bar{u}), \quad (v,\bar{v}) \to (-v,-\bar{v}).$$
 (3.2)

Indeed, it may be readily verified that this symmetry in unaffected by nonlinear SCC term. (We do not consider here large electric Reynolds numbers, where this nonlinear

4

term may result in a spontaneous symmetry breaking, see Yariv & Frankel 2016.) It follows that the drop does not move, U = 0. (This, of course, is the motivation for incorporating gravity effects in the first place.)

The third observation is that nonlinearities are introduced into the problem only through the boundary conditions, namely the charging condition governing the electrostatics and the shear-stress condition governing the flow. Since the governing differential equations are linear, the electric potentials and fluid velocities may be represented via appropriate eigenfunction expansions. In particular, the harmonic electric potential outside the drop may be written as a sum of spherical harmonics. Thus, using (2.6) and the axial symmetry we write

$$\varphi = -rP_1(\eta) + \sum_{n=1}^{\infty} A_n \frac{P_n(\eta)}{r^{n+1}},$$
(3.3)

wherein  $\eta = \cos \theta$  and  $P_n(\eta)$  are the Legendre polynomials of degree n. (Note that absence of a monopole term, in accordance with (3.1).) Because of (2.5) and the requirement of regularity within the drop, the potential there is

$$\bar{\varphi} = -rP_1(\eta) + \sum_{n=1}^{\infty} A_n r^n P_n(\eta).$$
(3.4)

In the absence of SCC (i.e. for Re = 0) the solution of the electrostatic problem is trivial, involving only the Legendre polynomial of the first degree (Melcher & Taylor 1969)

$$\varphi = -\left(r + \frac{1-R}{2+R}r^{-2}\right)\cos\theta, \quad \bar{\varphi} = -\frac{3}{2+R}r\cos\theta.$$
(3.5)

In the presence of SCC, expansions (3.3)–(3.4) generally consist of an infinite number of terms.

### 4. Weak fields

We focus here upon the case where the applied field is weak, in the sense that the electrohydrodynamic scale (2.2) is small compared with the characteristic settling velocity  $\mathcal{U}^*$ :

$$W \ll 1. \tag{4.1}$$

The leading-order flow field is therefore that associated with drop settling in the absence of any electrohydrodynamic effects due to a prescribed external force. Since this field may be considered as known, the SCC term in (2.7) becomes *linear* in the field, as is then the entire leading-order electrostatic problem.

Given definition (2.1) of the velocity scale, the drop settles at leading order with a unit speed (i.e. U = 1 in (2.12)). Within approximation (4.1) the leading-order 'electrohydrodynamic' correction to the velocity field is animated by the electrical shear stresses associated with the leading-order electric-field distribution. Since the hydrodynamic force associated with the leading-order flow already balances the external force due to gravity, the electrohydrodynamic correction must result in a nil hydrodynamic force. Defining

$$U = 1 + W\tilde{U} + \cdots . \tag{4.2}$$

The correction  $\tilde{U}$  to the settling velocity is set by this *force-free* condition. Our goal is the calculation of this correction. Note that  $\tilde{U}$  represents a normalization by the electro-hydrodynamic velocity scale (2.2).

# E. Yariv and Y. Almog

The O(W) electrohydrodynamic flow is governed by the continuity and Stokes equations, impermeability and velocity-continuity conditions at r = 1 (cf. (2.9)–(2.10)), far-field approach to  $-\tilde{U}\hat{\imath}$  (cf. (2.12)), and the force-free condition. It is driven by an inhomogeneous shear-stress condition (see (2.11)) associated with the distribution  $-q (\partial \varphi / \partial \theta)_{r=1}$  of electric shear stresses. (Hereafter q and  $\varphi$  refer to the respective leading-order quantities.)

Our interest lies in the electrohydrodynamic correction to the settling speed, rather than the detailed flow field associated with it. Using the reciprocal theorem of Stokes flow (Happel & Brenner 1965), this correction may be obtained as a linear functional of the electric-stress distribution. Thus, making use of the general result obtained by Nadim, Haj-Hariri & Borhan (1990) we obtain here

$$\tilde{U} = \frac{1}{8\pi} \frac{M}{M+3/2} \hat{\imath} \cdot \oint_{r=1} \mathrm{d}A \, \hat{\boldsymbol{e}}_{\theta} q \frac{\partial \varphi}{\partial \theta}.$$
(4.3)

Upon substituting (2.8) and reverting to  $\eta$  as the integration variable,

$$\tilde{U} = -\frac{1}{4} \frac{M}{M+3/2} \int_{-1}^{1} (1-\eta^2) \left( \frac{\partial \varphi}{\partial r} - S^{-1} \frac{\partial \bar{\varphi}}{\partial r} \right) \frac{\partial \varphi}{\partial \eta} \Big|_{r=1} \, \mathrm{d}\eta.$$
(4.4)

Substituting (3.3)–(3.4) and making use of (5.4) and (5.6) in conjunction with the orthogonality of the Legendre polynomials eventually furnishes the desirable formula

$$\frac{M+3/2}{M}\tilde{U} = \frac{6-S^{-1}}{15}A_2 + \sum_{n=1}^{\infty} \frac{n+1+nS^{-1}}{2(2n+1)}A_n \left[\frac{(n+1)(n+2)}{2n+3}A_{n+1} - \frac{n(n-1)}{2n-1}A_{n-1}\right].$$
 (4.5)

It is worth emphasising that, in the limit (4.1), the electric potential satisfies a linear problem while the drop velocity is quadratic in that potential. The assumption, made in the problem formulation, that the applied field points in the settling-direction  $\hat{\imath}$  (parallel to gravity for  $\bar{\rho}^* > \rho^*$ , anti-parallel to it for  $\bar{\rho}^* < \rho^*$ ) is accordingly non-restrictive. Indeed, an applied field in the opposite direction would simply reverse the electric-field distribution, resulting in an identical value of  $\tilde{U}$ .

# 5. Electrostatic problem

In the drop-fixed reference system, where at large r the velocity tends to  $-\hat{\imath}$ , the interfacial velocity is (Happel & Brenner 1965)

$$v = \frac{M}{2(1+M)}\sin\theta.$$
(5.1)

We accordingly consider the electrostatic problem resulting from substitution of the leading-order distribution (5.1) into the SCC term. Thus, substitution of (3.3)–(3.4) and (5.1) into the respective left- and right-hand sides of (2.7) followed by integration readily yields

$$\int_{-1}^{\eta} \left[ (1-R)P_1(t) + \sum_{n=1}^{\infty} (n+1+nR)A_n P_n(t) \right] dt = \frac{\mathscr{R}}{2} (1-\eta^2)q,$$
(5.2)

wherein the electric Reynolds number and viscosity ratio appear through the single group

$$\mathscr{R} = \frac{M}{1+M}Re.$$
(5.3)

 $\mathbf{6}$ 

#### The settling velocity of spherical drops in a uniform electric field

Use of the following form of the Legendre equation

$$n(n+1)\int_{-1}^{\eta} P_n(t) \,\mathrm{d}t = -(1-\eta^2)P_n'(\eta) \tag{5.4}$$

(wherein the prime denote differentiation) and substitution of (2.8) gives

$$\frac{1-R}{2}P_1'(\eta) + \sum_{n=1}^{\infty} \frac{n+1+nR}{n(n+1)} A_n P_n'(\eta) = \frac{\mathscr{R}}{2} \left(\frac{\partial\varphi}{\partial r} - S^{-1}\frac{\partial\bar{\varphi}}{\partial r}\right).$$
(5.5)

Substitution of (3.3)-(3.4) into the right-hand side and making use of the identity

$$P_n(\eta) = \frac{P'_{n+1}(\eta) - P'_{n-1}(\eta)}{2n+1},$$
(5.6)

in conjunction with the orthogonality of the derivatives of the Legendre polynomials (with respect to  $1 - \eta^2$ ), yields

$$A_{n} + \frac{n(n+1)\mathscr{R}}{2(n+1+nR)} \left\{ \frac{n+(n-1)S^{-1}}{2n-1} A_{n-1} - \frac{n+2+(n+1)S^{-1}}{2n+3} A_{n+1} \right\} = \begin{cases} \frac{R-1}{R+2}, & n=1, \\ \frac{S^{-1}-1}{3+2R}\mathscr{R}, & n=2, \\ 0, & n>2, \end{cases}$$
(5.7)

where we take  $A_0 = 0$ . We have therefore obtained an infinite tridiagonal system governing the coefficients  $\{A_n\}_{n=1}^{\infty}$ .

## 6. Small Re

For small Re an approximate solution is readily obtained by linearising about (3.5), where all coefficients except  $A_1$  vanish. Thus, at O(Re) we find a nonzero  $A_2$ . The O(Re)excess velocity (4.5) is proportional to the product of these two coefficients, giving

$$\tilde{U} = -\frac{18M^2(RS-1)(RS+S-1/3)}{5(1+M)(3+2M)(2+R)^2(3+2R)S^2}Re,$$
(6.1)

in agreement with equation (34) of Xu & Homsy (2006). For  $RS > 1 \tilde{U}$  is negative, while for 1/3 < RS < 1 it is positive. For  $RS < 1/3 \tilde{U}$  is positive if RS > 1/3 - S (which is always the case for S > 1/3) and negative otherwise (in which case S < 1/3). In the limit of a gas bubble, where R = 0 and  $M = \infty$ ,

$$\tilde{U} = \frac{3(S - 1/3)}{20S^2} Re.$$
(6.2)

For a gas bubble  $\bar{\epsilon}^*$  is approximately that of vacuum meaning that  $S \ge 1$ ;  $\tilde{U}$  is therefore positive.

Since the present approximation scheme, where Re is arbitrary and  $W \ll 1$ , is 'orthogonal' to that made by Xu & Homsy (2006), where W is arbitrary and  $Re \ll 1$ , the agreement with Xu & Homsy (2006) may appear surprising. To understand it, it is useful to consider carefully the small-Re limit of Xu & Homsy, keeping in mind the physical origin of the pertinent terms. The leading-order flow in that limit is a superposition of two components. The first, associated with 'pure settling,' is independent of the electric field; it is therefore identical to the leading-order flow in the present approximation scheme. The second 'purely electrohydrodynamic' component, is proportional to W (i.e.

7

#### E. Yariv and Y. Almog

to the square of the applied-field magnitude). Since the leading-order surface-charge density is proportional to the applied field, the SCC term associated with the leading-order product of tangential velocity surface-charge density also decomposes into two parts, one proportional to the applied field, the other to its cube. The second part, however, simply represents SCC in the absence of gravity; as such, it does not affect the drop velocity (see (3.2) et seq.). The perturbation to the electric potential (and to the surface charge) due to SCC is accordingly proportional to the field. The resulting modification to the drop velocity is driven by quadratic interaction of that perturbation with the leadingorder electric potential, which is also proportional to the field. The velocity modification is accordingly proportional to the field square, or, in dimensionless terms, to W — just as though a perturbation in W was carried out from the outset.

# 7. Finite Re

Consider now the difference equation (5.7) for arbitrary Re. While no analytic solution appears generally possible,<sup>†</sup> useful information may be extracted by considering the largen asymptotic limit, where this equation becomes

$$A_n = \frac{n}{2\alpha} \left[ 1 + O(n^{-1}) \right] \left( A_{n+1} - A_{n-1} \right), \tag{7.1}$$

in which

$$\alpha = \frac{2S(1+R)}{\mathscr{R}(1+S)}.$$
(7.2)

This homogenous second-order equation possesses two solutions. To ensure convergence of the original series (3.3), only the solution that decays at large n is admissible. It may then be verified that

$$A_n \sim \text{constant} \times \frac{(-)^n}{n^{\alpha}} \quad \text{as} \quad n \to \infty,$$
 (7.3)

wherein the asymptotic correction is of relative order  $n^{-1}$ . Considering the summation in (4.5), the series converges if and only if  $\alpha > 1/2$ , i.e. when

$$Re < \frac{4S(1+R)(1+M)}{M(1+S)}.$$
(7.4)

For an arbitrary Re satisfying (7.4) the system (5.7) is solved using controlled truncation, where the infinite equation set is approximated by a finite set of N equations. Thus, making use of the leading-order approximation (7.3) we replace  $A_{N+1}$  in the N-th equation by  $-A_N/(1+1/N)^{\alpha}$ . In calculating the series (4.5) we estimate the 'tail' contribution from  $\{A_n\}_{n=N+1}^{\infty}$  using the above leading-order approximation. This provides a rapid convergence scheme even when Re is close to the critical value specified by (7.4).

Note that the value of M enters (5.7) only through the rescaled electric Reynolds number  $\mathscr{R}$ . Similarly, (4.5) provides the rescaled velocity  $(M + 3/2)\tilde{U}/M$  as a series which is independent of M. It follows that we may obtain results valid for all M using a single calculation. Such a calculation is illustrated in figure 1 showing the rescaled velocity as a function of  $\mathscr{R}$  for R = 0 and S = 1, where the critical value of  $\mathscr{R}$  is 2. Also shown is the corresponding small-Re approximation,

$$\tilde{U} = \frac{M^2}{5(1+M)(3+2M)} Re,$$
(7.5)

† We have managed to obtain closed-form analytic solution for the case R=0 and S=1 when  $\mathscr{R}=1,\,1/2,\,1/3,\ldots$ 



FIGURE 1. Rescaled velocity  $(M + 3/2)\tilde{U}/M$  as a function of  $\mathscr{R}$  for R = 0 and S = 1. The thin line depicts the corresponding small-Re approximation (7.5) of slope 1/10. The critical value  $\mathscr{R} = 2$  is indicated.

obtained from (6.1). Note the non-monotonic variation with the electric Reynolds number and, in particular, the transition from a positive to negative  $\tilde{U}$ .

# 8. Experimental relevance

The key assumption of the present approximation scheme is that the ratio W of electric and gravity forces is small while the electric Reynolds number is O(1). It is also assumed that the drop is approximately spherical and that inertia plays a negligible role. We here illustrate that these assumptions are indeed compatible with realistic experimental systems.

We first note that, while W is proportional to the square of the applied-field magnitude  $E^*$ , the electric Reynolds number is independent of it. Thus, provided the applied field is sufficiently weak W can always be made sufficiently small without affecting Re. It therefore remains to verify that Re can indeed reach O(1) values while the viscous Reynolds number remains small.

Recall also that, in the absence of an electric field, a settling drop does not deform in the Stokes-flow régime, regardless of the value of the Capillary number (Levich 1962). Drop deformation thus occurs at leading-order due to the O(W) stresses animated by the electric field, and accordingly scales as the product of W and the appropriate Capillary number Ca. The assumption of a nearly spherical drop is trivially satisfied even for O(1)Capillary numbers.

An even stricter demand from that of approximate sphericity is that the SCC-induced O(W) perturbation to the settling speed, calculated herein, dominates the comparable perturbation due to deviation from sphericity. This ensures that the velocity perturbation calculated in the present approximation scheme could be directly compared to that measured experimentally. Since drop deformation results in an O(WCa) correction to the settling speed, this requires that the Capillary number itself be small.

Plugging the velocity scale (2.1) into (2.4) we see that the electric Reynolds number

is of order

$$\frac{\epsilon^*|\bar{\rho}^* - \rho^*|g^*a^*}{\mu^*\sigma^*},\tag{8.1}$$

linear in drop size. The capillary number Ca is  $\mu^* \mathcal{U}^* / \gamma^*$ , wherein  $\gamma^*$  the interfacialtension coefficient. Since the velocity scale (2.1) is set by gravity, it coincides here with the Bond number, namely

$$Ca = \frac{|\bar{\rho}^* - \rho^*| g^* a^{*2}}{\gamma^*},$$
(8.2)

and scales as the square of drop size. The viscous Reynolds number is

$$\frac{\rho^* |\bar{\rho}^* - \rho^*| g^* a^{*3}}{{\mu^*}^2},\tag{8.3}$$

proportional to the cube of drop size.

To estimate the above three numbers consider the experiments of Xu & Homsy (2006), where a millimetric-size PMM drop was suspended in castor oil. This choice of liquids was motivated by the large density difference,  $\bar{\rho}^* - \rho^* \approx 40 \text{ kg m}^{-3}$ , which allows for a significant settling speed. For castor oil Xu & Homsy (2006) provide the values  $\rho^* \approx$ 960 kg m<sup>-3</sup> and  $\mu^* \approx 1.4 \text{ kg m}^{-1} \text{ s}^{-1}$ , as well as a dielectric constant of about 5. There is a significant uncertainty regarding the value of castor oil conductivity. We here use the estimate  $\sigma^* \approx 10^{-11} \text{ S m}^{-1}$  provided by Vizika & Saville (1992). (In their comparison with theoretical predictions, Xu & Homsy postulate the even smaller value  $2.4 \times 10^{-12} \text{ S m}^{-1}$ .)

Taking  $a^* = 10^{-3}$  m and making use of the above-mentioned values we find from (8.1) that the electric Reynolds number is about unity. The Bond number, estimated using (8.2) and the value  $\gamma^* \approx 5 \times 10^{-3}$  N m<sup>-1</sup> provided by Xu & Homsy (2006), is about 0.1. The Reynolds number (8.3) is of order  $10^{-4}$ . These values support our approximation scheme. If silicone oil is used instead of castor oil as the suspending fluid, the conductivity reduces to about  $10^{-12}$  S m<sup>-1</sup>. Since the density difference  $\bar{\rho}^* - \rho^* \approx 30$  kg m<sup>-3</sup> is comparable to that above, this choice can lead to even larger values of Re.

#### 9. Concluding remarks

We have considered the electrohydrodynamic problem of drop settling in the presence of an electric field, accounting for SCC. By focusing upon weak fields we have obtained a linear problem governing the electric potential, valid for all values of Re. Once the electrostatic problem is solved, the excess drop velocity (relative to that in the absence of a field) may be obtained as a linear functional of the associated electric shear stress. Our approach provides a different perspective from that of Xu & Homsy (2006), who considered small electric Reynolds numbers but fields which are not weak. Remarkably, it turns out that despite the present weak-field assumption our scheme reproduces at small Re the approximation obtained by Xu & Homsy (2006).

The linear electrostatic problem has been reduced to a difference equation governing the respective coefficients in a spherical-harmonics expansion of the electric potential. Using this expansion, the integral formula for the drop speed reduces to a single series, quadratic in these coefficients. Inspection reveals a singularity at a critical electric Reynolds number whose value is explicitly obtained in terms of the material ratios R, S and M. For electric Reynolds numbers smaller from the critical values we find a nonmonotonic variation of drop speed with the applied field-magnitude. In particular, we observe a transition from velocity enhancement at small Re to velocity decrement at larger Re values.

10

#### The settling velocity of spherical drops in a uniform electric field

The finite-Re singularity discovered herein and the trends observed in figure 1 illustrate the limitation of the small-Re approximation and motivate the respective nonlinear analysis of the problem for arbitrary values of W and Re. Since nonlinearity enters the flow problem only through the shear-stress condition (2.11), the velocity field may be conveniently expanded using the appropriate eigenfunction of the Stokes equations in spherical coordinates (Happel & Brenner 1965). Conditions (2.7) and (2.11) would then involve both the coefficients of such an expansion as well as those of expansion (3.3). This nonlinear analysis, and in particular the behaviour near the critical electric Reynolds number identified herein, is suggested as an open problem. An even more challenging problem arises when when the electric field in not aligned with the direction of gravity. This problem was recently analysed assuming a small electric Reynolds number (Bandopadhyay *et al.* 2016).

In both the pioneering paper of Xu & Homsy (2006) and the present contribution the quantity of interest is the modification to the settling velocity due to electric-field application. This concept can be easily generalised by considering the effect of ambient flow rather than gravity. In the absence of an electric field the drop is entrained by the flow, moving with a velocity given by Faxén's law. In the presence of an external electric field, the SCC-induced electric stresses result in a different drop velocity. The respective velocity modification may be calculated in principle using an analog of the present weakfield scheme, where appropriate use of the reciprocal theorem would provide it as a linear functional of the electric shear stresses. Since the electric stresses in the weak-field scheme are quadratic in the leading-order electric-potential distribution, and given the clear nonlinear dependence of that distribution upon Re (see (2.7)), it is evident that the velocity modification is nonlinear in the magnitude of the ambient flow. The well-known symmetry arguments of Stokes flow (Jeffrey 1996) are then inapplicable.

The simplest non-trivial scenario may be that of a drop in a simple shear flow (Vlahovska 2011). In the absence of an electric field, the symmetry arguments of Stokes flow preclude drop migration across the streamlines; in fact, the drop simply moves with the velocity of the ambient streamline passing through its centre (Kim & Karrila 2005). In the presence of an electric field, however, the breakdown of these arguments imply the possibility of migration across streamlines. This may be the case even when the field is applied in the flow direction, because of the asymmetry introduced by the shear-direction. (This asymmetry enters the problem through the counterpart of the interfacial-velocity profile (5.1) which, for a drop suspended in a shear flow, lacks axial symmetry.) There is some conceptual similarity of this field-induced nonlinear mechanism for cross-streamline migration and that due to Marangoni stresses (Pak, Feng & Stone 2014), where nonlinearity stems from solute advection.

We are grateful to Ory Schnitzer for suggesting this problem. This work was supported by the Israel Science Foundation (grant no. 184/12).

#### REFERENCES

BANDOPADHYAY, A., MANDAL, S., KISHORE, N. K. & CHAKRABORTY, S. 2016 Uniform electricfield-induced lateral migration of a sedimenting drop. J. Fluid Mech. **792**, 553–589.

- FENG, J. Q. 1999 Electrohydrodynamic behaviour of a drop subjected to a steady uniform electric field at finite electric Reynolds number. Proc. Roy. Soc. London. A 455 (1986), 2245–2269.
- HAPPEL, J. & BRENNER, H. 1965 Low Reynolds Number Hydrodynamics. Englewood Cliffs, N. J.: Prentice-Hall.

JEFFREY, D. J. 1996 Some basic principles in interaction calculations. In Sedimentation of

small particles in a viscous fluid (ed. E. M. Torry), chap. 4, pp. 97–124. Southampton: Computational Mechanics.

KIM, S. & KARRILA, S. J. 2005 Microhydrodynamics: Principles and Selected Applications. Dover, Mineola, NY.

LANAUZE, J. A., WALKER, L. M. & KHAIR, A. S. 2015 Nonlinear electrohydrodynamics of slightly deformed oblate drops. J. Fluid Mech. 774, 245–266.

LEVICH, V. G. 1962 Physicochemical Hydrodynamics. Englewood Cliffs, N.J.: Prentice-Hall.

- MELCHER, J. R. & TAYLOR, G. I. 1969 Electrohydrodynamics: a review of the role of interfacial shear stresses. Ann. Rev. Fluid Mech. 1 (1), 111–146.
- NADIM, A., HAJ-HARIRI, H. & BORHAN, A. 1990 Thermocapillary migration of slightly deformed droplets. *Particul. Sci. Technol.* 8 (3-4), 191–198.
- PAK, O. S., FENG, J. & STONE, H. A. 2014 Viscous marangoni migration of a drop in a Poiseuille flow at low surface Péclet numbers. J. Fluid Mech. **753**, 535.
- RIVETTE, N. J. & BAYGENTS, J. C. 1996 A note on the electrostatic force and torque acting on an isolated body in an electric field. *Chem. Engng Sci.* **51** (23), 5205–5211.
- TAYLOR, G. 1966 Studies in electrohydrodynamics. I. The circulation produced in a drop by electrical field. *Proc. Roy. Soc. London A* **291** (1425), 159–166.
- VIZIKA, O. & SAVILLE, D. A. 1992 The electrohydrodynamic deformation of drops suspended in liquids in steady and oscillatory electric fields. J. Fluid Mech. 239 (1), 1–21.
- VLAHOVSKA, P. M. 2011 On the rheology of a dilute emulsion in a uniform electric field. J. Fluid Mec. 670, 481–503.
- Xu, X. & Homsy, G. M. 2006 The settling velocity and shape distortion of drops in a uniform electric field. J. Fluid Mech. 564, 395–414.
- YARIV, E. 2006 "Force-free" electrophoresis? Phys. Fluids 18, 031702.
- YARIV, E. & FRANKEL, I. 2016 Electrohydrodynamic rotation of drops at large electric reynolds numbers. J. Fluid Mech. 788, R2.